

## **ANFA Nonwovens Conference 2019**

# **Innovative Application of Non-woven Textiles on Industrial Wastewater Biological Treatment**

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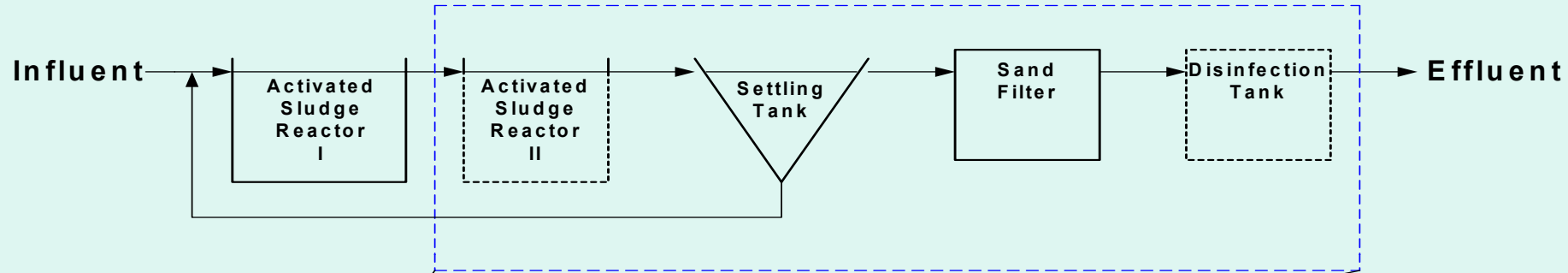
Director of Water Technology Research Division,  
Material and Chemical Engineering research Labs,  
Industrial Technology Research Institute.

<http://www.itriwater.org.tw/>

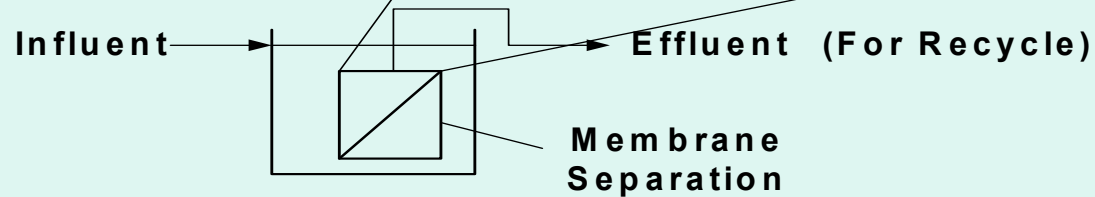
<http://www.itri.org.tw/>

# ASP vs. MBR

## Activated Sludge Process



## Membrane Bioreactor Process



Note: from Gunder & Krauth, Wat. Sci. tech., 40(4-5), 311-320.

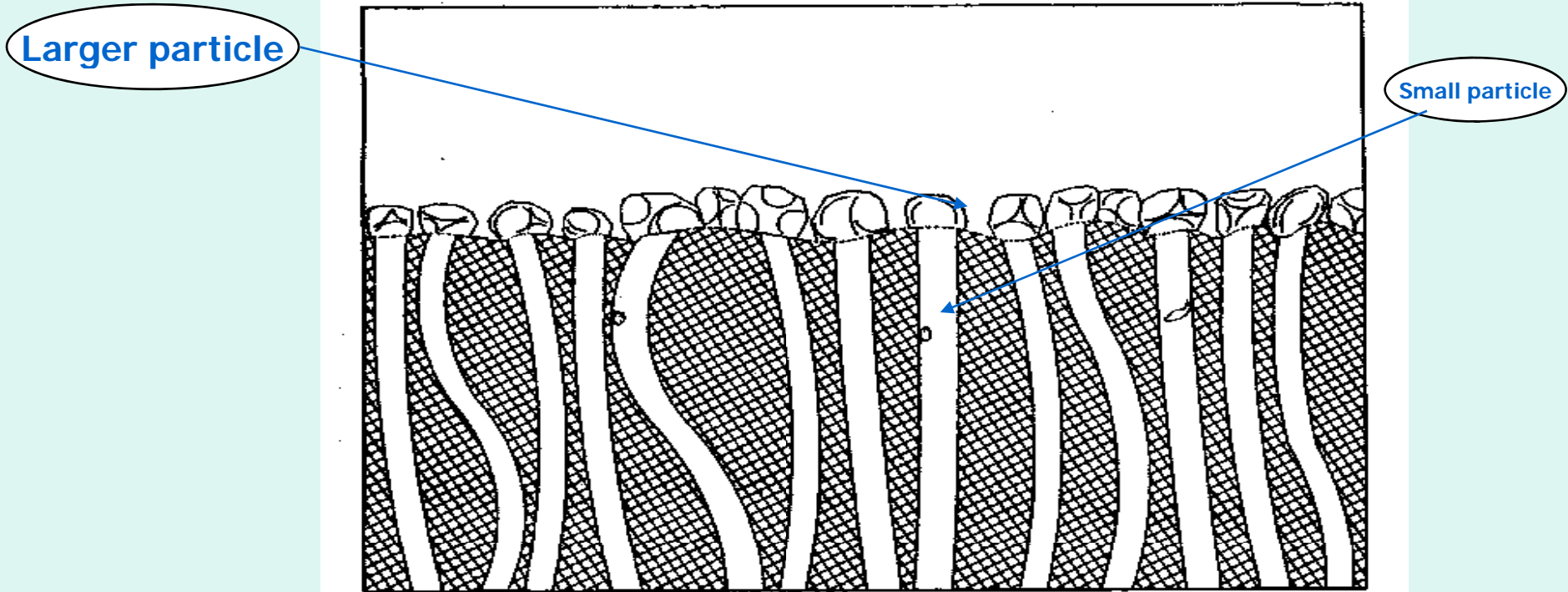
# Commercial Membrane Material

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- The membrane materials commercially used in MBR process include ceramics and both unmodified and surface modified polymeric materials, called microporous membrane.
- The pore size of these membrane materials are usually in the  $0.02\mu\text{m}\sim 0.5\mu\text{m}$  range.

# Filtration Characteristics of Microporous Membrane

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*Figure 2.4. Schematic of screen filter, which retains particles on its surface.*

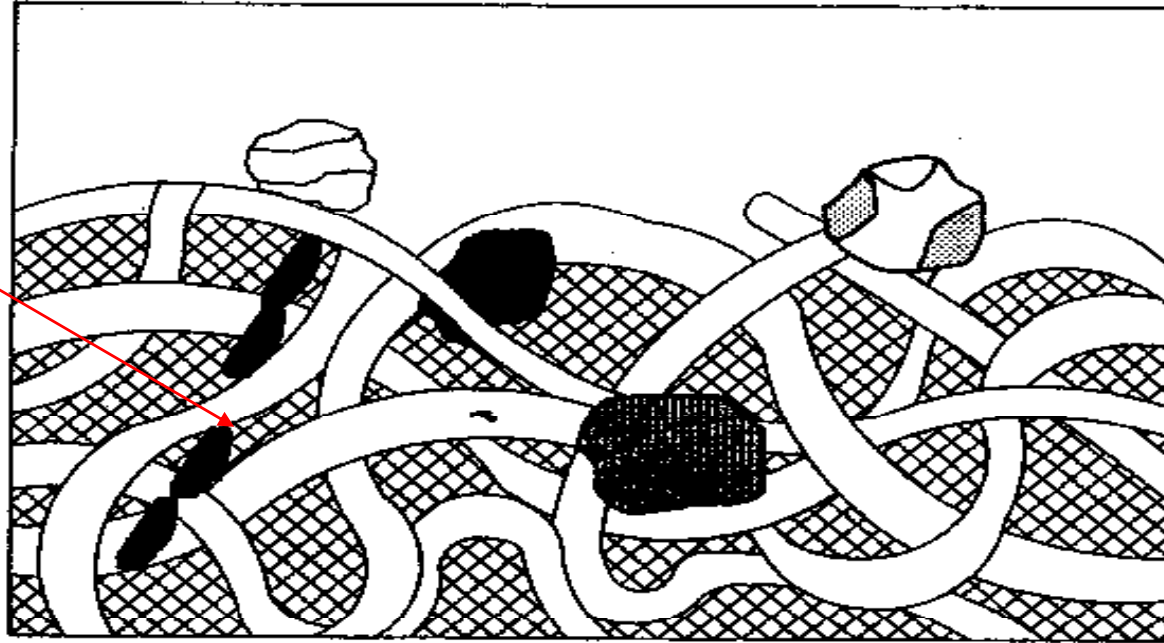
# Non-woven Fabric Material

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- Non-woven fibrous materials are composed of random network of overlapping fibers which create multiply connected pores through which the fluid can flow.
- It is also a less expensive filter material for water treatment.

# Filtration Characteristics of Non-woven Membrane

The size of particle  
small than that of pore  
can be collected



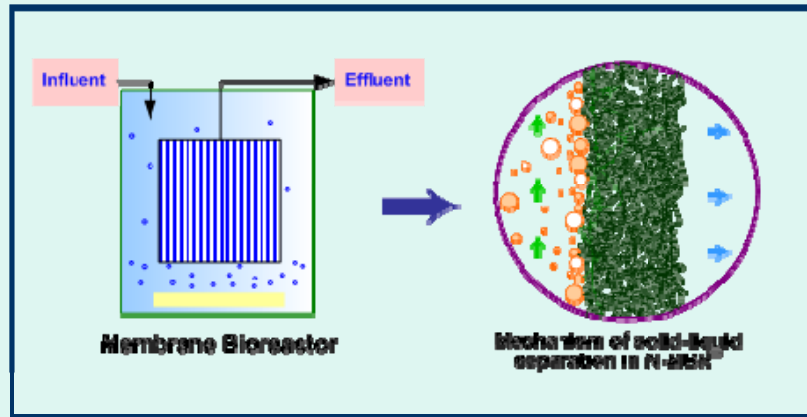
**Figure 2.2.** Schematic of depth filter, showing the randomly oriented fibers trapping particles on its surface and within its matrix.

# Filtration Characteristics of Non-woven Fabric Membrane

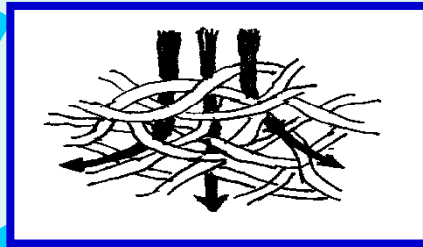
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- In non-woven fabric membrane, particle collection mechanisms include **inertial impaction, interception and Brownian diffusion** etc. Particles with size smaller than the average pore size can also be collected totally or partially due to **Brownian diffusion** which is especially the dominant particle collection mechanism for ultra-fine particles.

# Non-woven MBR System



Variable pore size



3D structure

Good chemical stability

High porosity

# Contribution to Membrane Fouling in MBR System

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- For **microporous** membrane, the main components of activated sludge system that contributed to membrane fouling are **soluble microbial product and small size colloid**.
- As for larger pore size **non-woven** membrane, **suspended sludge floc particle** may be expected to have a profound influence on membrane fouling.

# Advantages of MBRs

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- Stable operation and superior effluent quality
- Easy revamping of existing plants
- Easy process control
- Small footprint
- Less sludge production

## Serious concerns

- Energy consumption of scouring aeration of membrane surface
- Cost of chemical cleaning of membrane to remove fouling

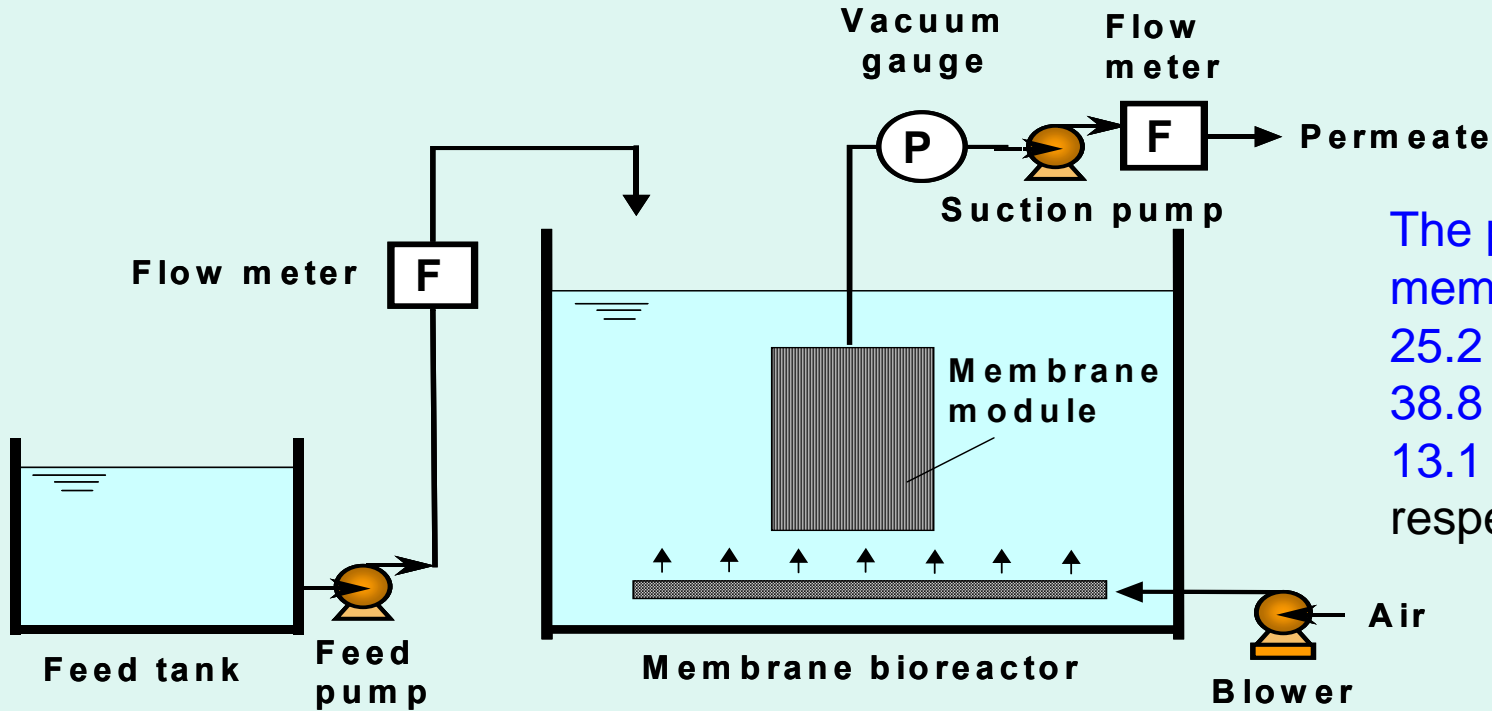
# Non-woven MBR System

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## Unique Features

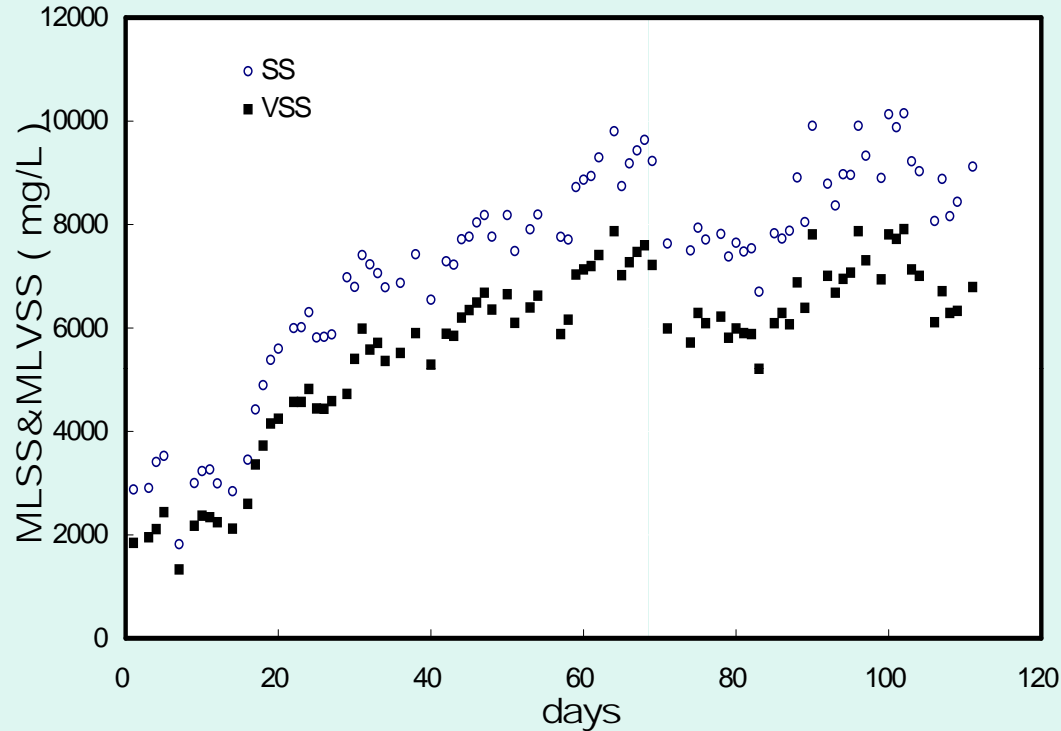
- Controllable pore size distribution
- Easy fabrication of membrane module
- High specific permeate flux at low transmembrane pressure

# Non-woven MBR Pilot Test



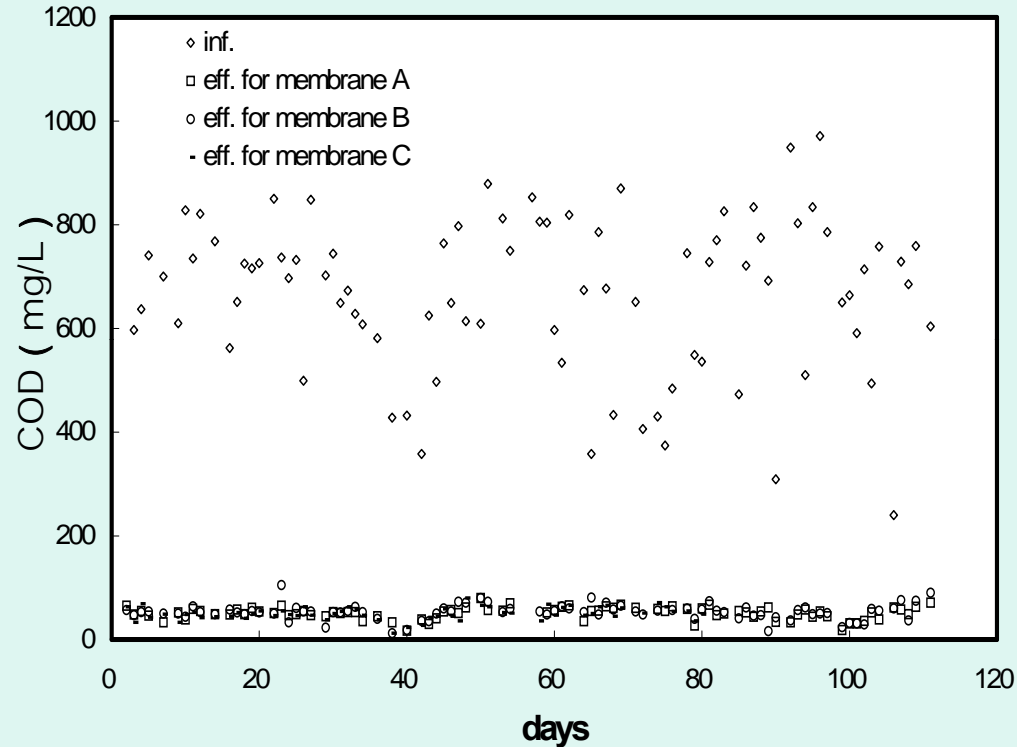
The pore size of non-woven membrane tested was 25.2  $\mu\text{m}$  (membrane A), 38.8  $\mu\text{m}$  (membrane B), and 13.1  $\mu\text{m}$  (membrane C) respectively.

# Non-woven MBR Pilot Test



Change of MLSS and MLVSS concentration in submerged non-woven membrane bioreactor during the operation period. Experimental conditions: membrane type (membrane A), aeration intensity ( $0.01 \text{ m}^3/\text{m}^2 \cdot \text{sec}$ ), initial flux ( $0.2 \text{ m}^3/\text{m}^2 \cdot \text{day}$ )

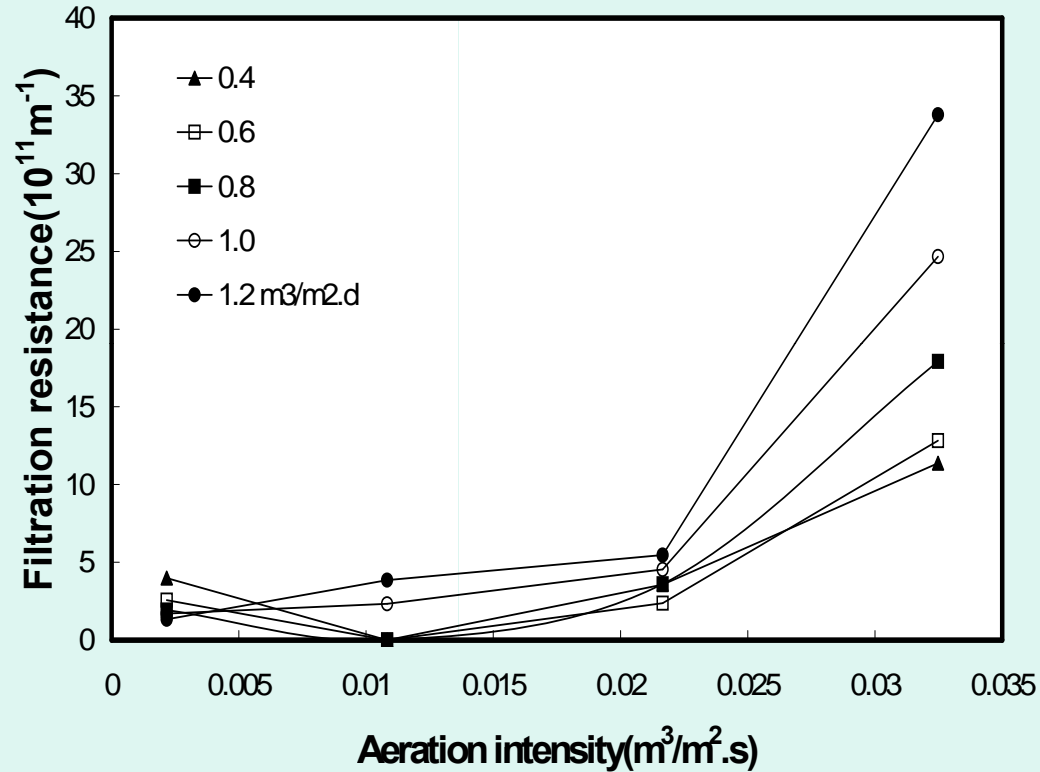
# Non-woven MBR Pilot Test



Influent and effluent COD in the submerged non-woven membrane bioreactor during the operation period

# Non-woven MBR Pilot Test

## Aeration intensity effect



Change of filtration resistance with aeration intensity at different initial flux.  
Experimental conditions: membrane type (membrane A), MLSS (5,000 mg/L)

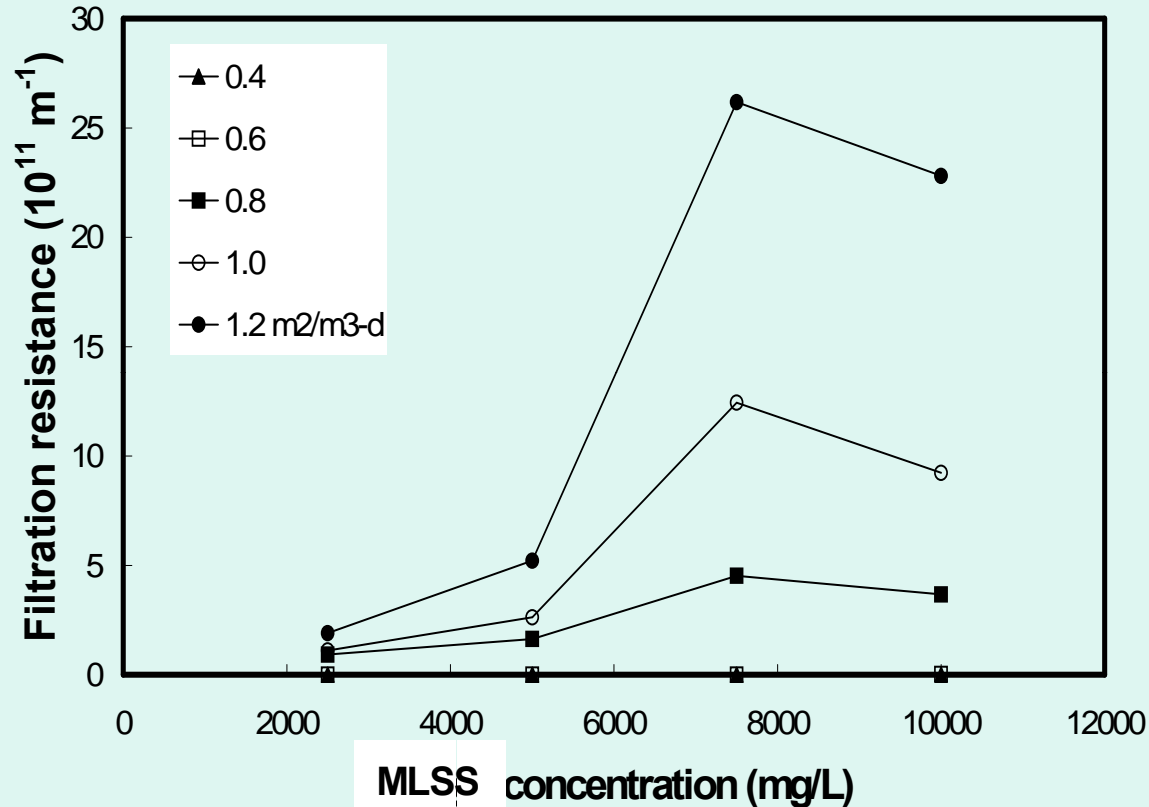
# Aeration Intensity Effect

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- It is shown that the filtration resistance increased with increasing aeration intensity when initial flux was set at the value higher than  $0.8 \text{ m}^3/\text{m}^2.\text{day}$  ( $33 \text{ L}/\text{m}^2.\text{hr}$ ). However, there existed a minimum filtration resistance at aeration intensity of  $0.01 \text{ m}^3/\text{m}^2.\text{sec}$  when initial flux was lower than  $0.8 \text{ m}^3/\text{m}^2.\text{day}$  and filtration resistance was nearly zero.

# Non-woven MBR Pilot Test

## MLSS effect



Change of filtration resistance with MLSS at different initial flux. Experimental conditions: membrane type (membrane A), aeration intensity ( $0.01 \text{ m}^3/\text{m}^2\cdot\text{sec}$ )

# Non-woven MBR Pilot Test

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- The filtration resistance was independent of MLSS at initial flux of 0.4 and 0.6  $\text{m}^3/\text{m}^2\cdot\text{day}$  .
- However, the filtration resistance increased with the increasing of the MLSS, then to a maximum value around 7,600 mg/L at higher initial flux. This trend was more evident when the initial flux was larger than 0.8  $\text{m}^3/\text{m}^2\cdot\text{day}$  (33  $\text{L}/\text{m}^2\cdot\text{hr}$  ).

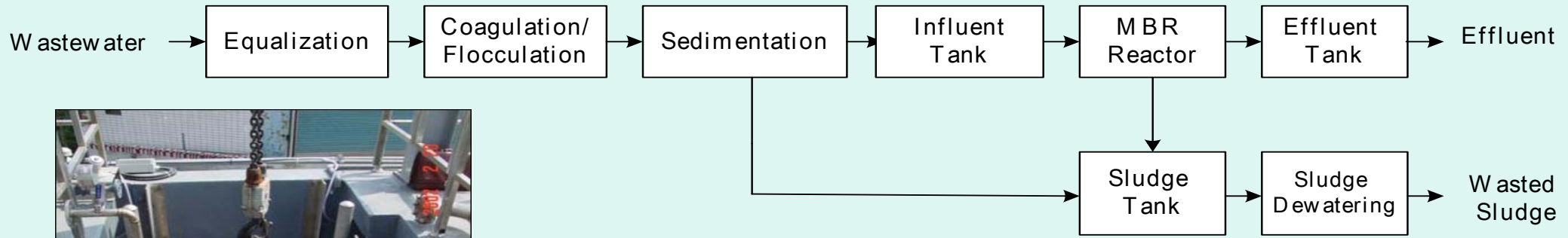
# The Difference Between Microporous and Non-woven Membrane System

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- In the microporous membrane systems, even with very strong aeration intensity, the aeration intensity has no effect on filtration resistance beyond some critical value.
- However, there exists a minimum and zero filtration resistance at some case in our non-woven membrane bioreactor system.

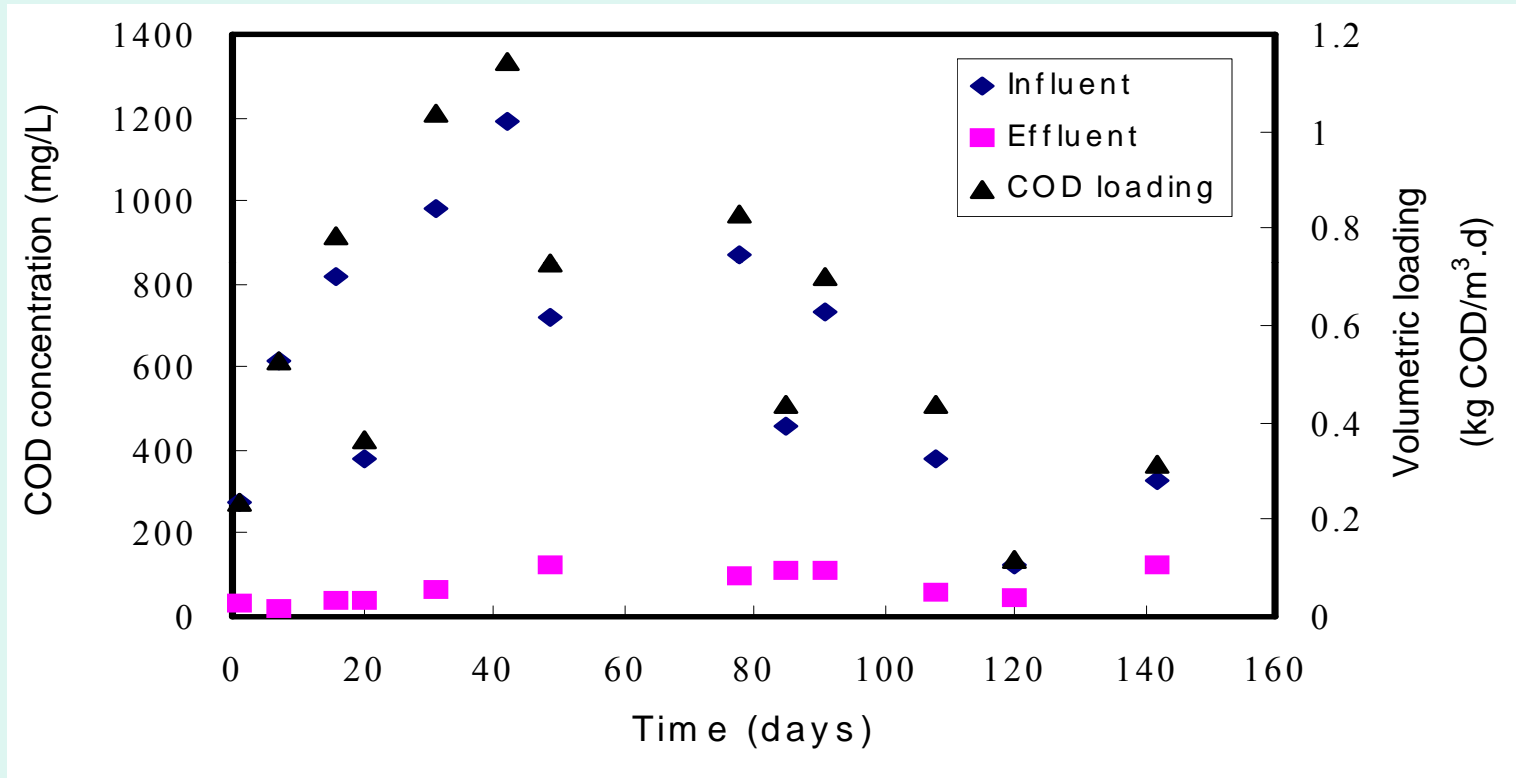
# **Industrial Wastewater Treatment**

# Wastewater Treatment Process



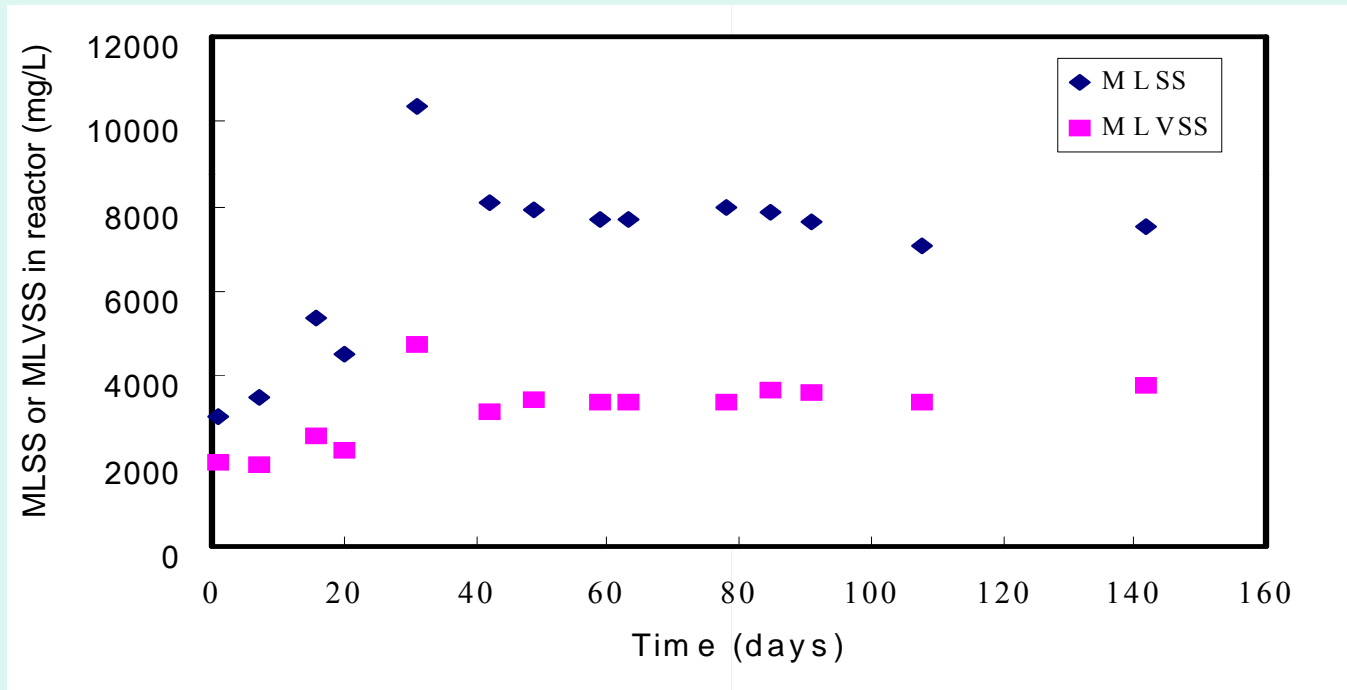
# Personal care product wastewater

## Influent and Effluent COD of Non-woven MBR



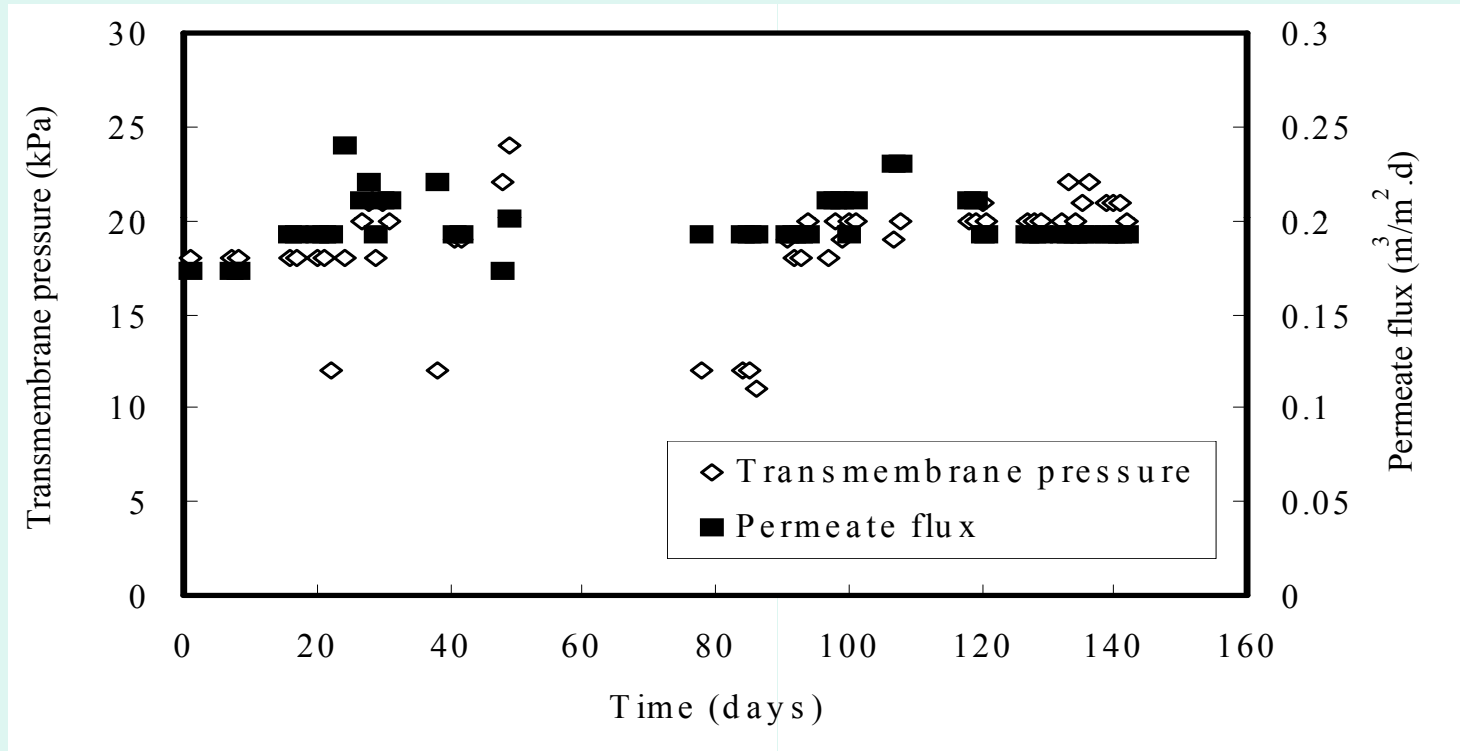
# Personal care product wastewater

## MLSS Concentration in non-woven MBR Reactor



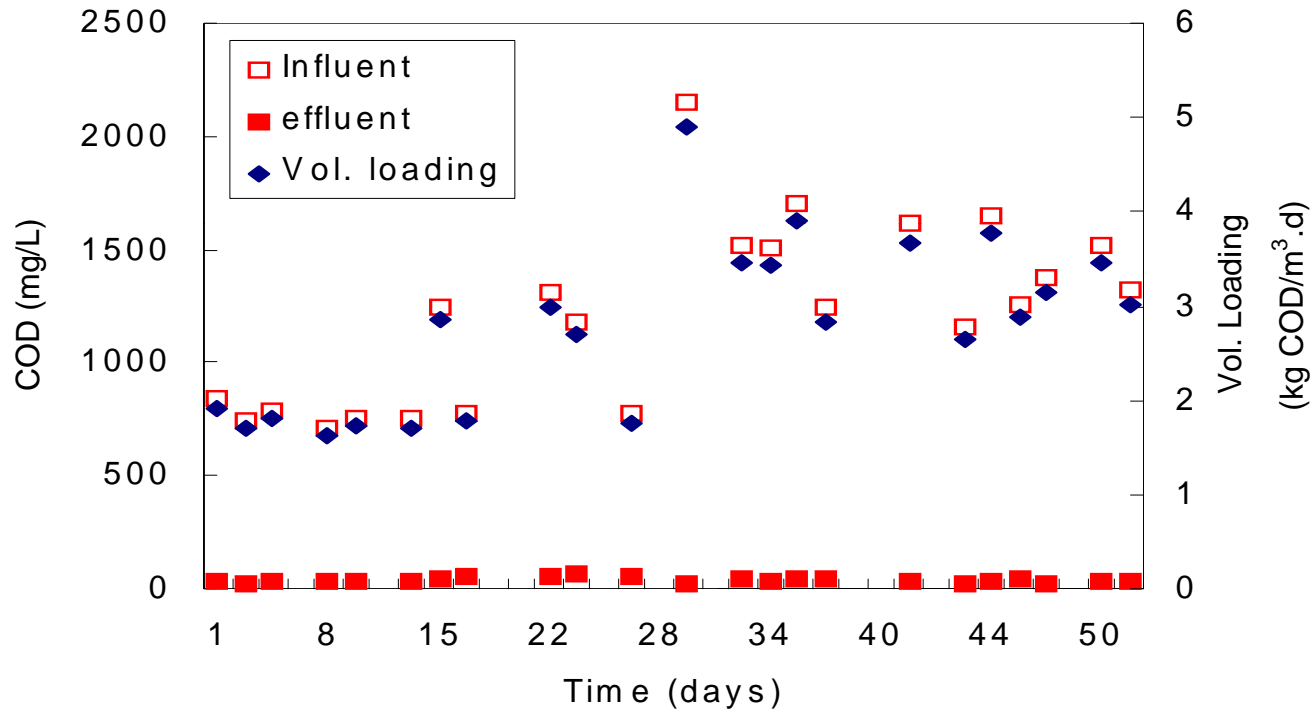
# Personal care product wastewater

## Operation Pressure and Permeate Flux



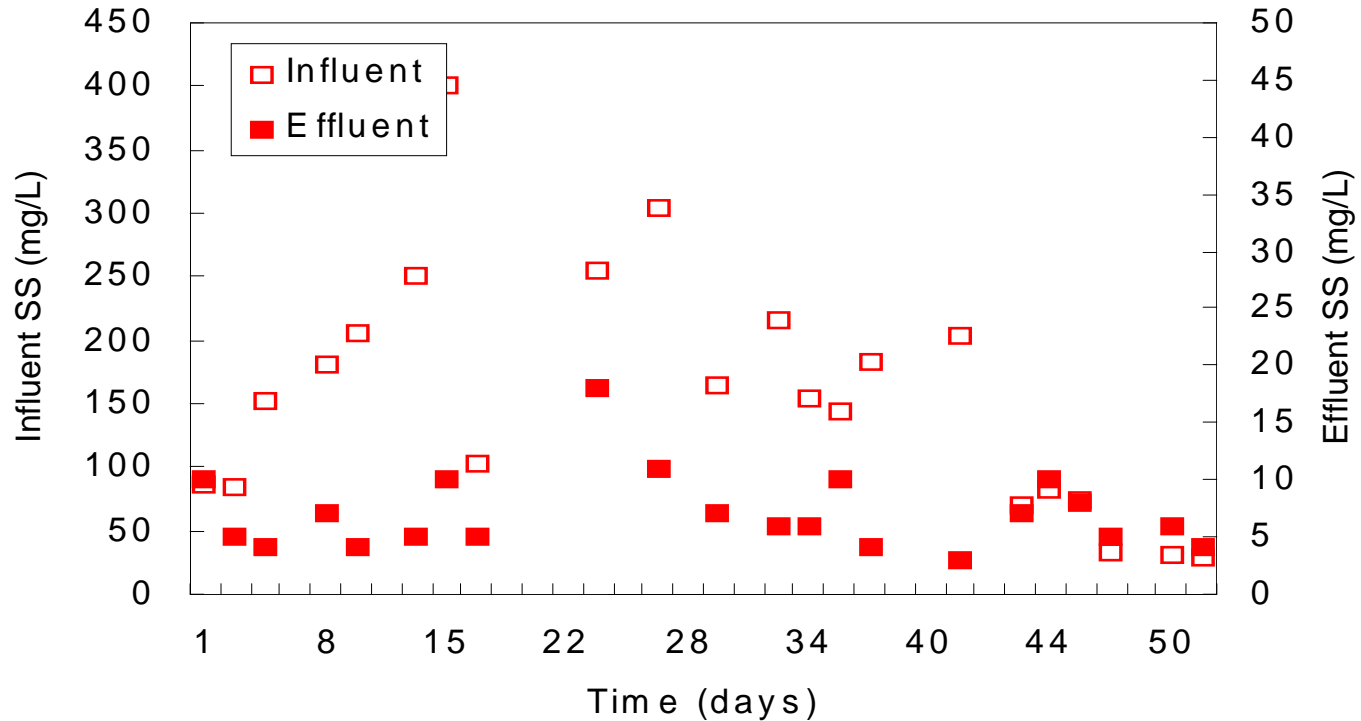
# Food Product Wastewater

## Influent and Effluent COD of Non-woven MBR



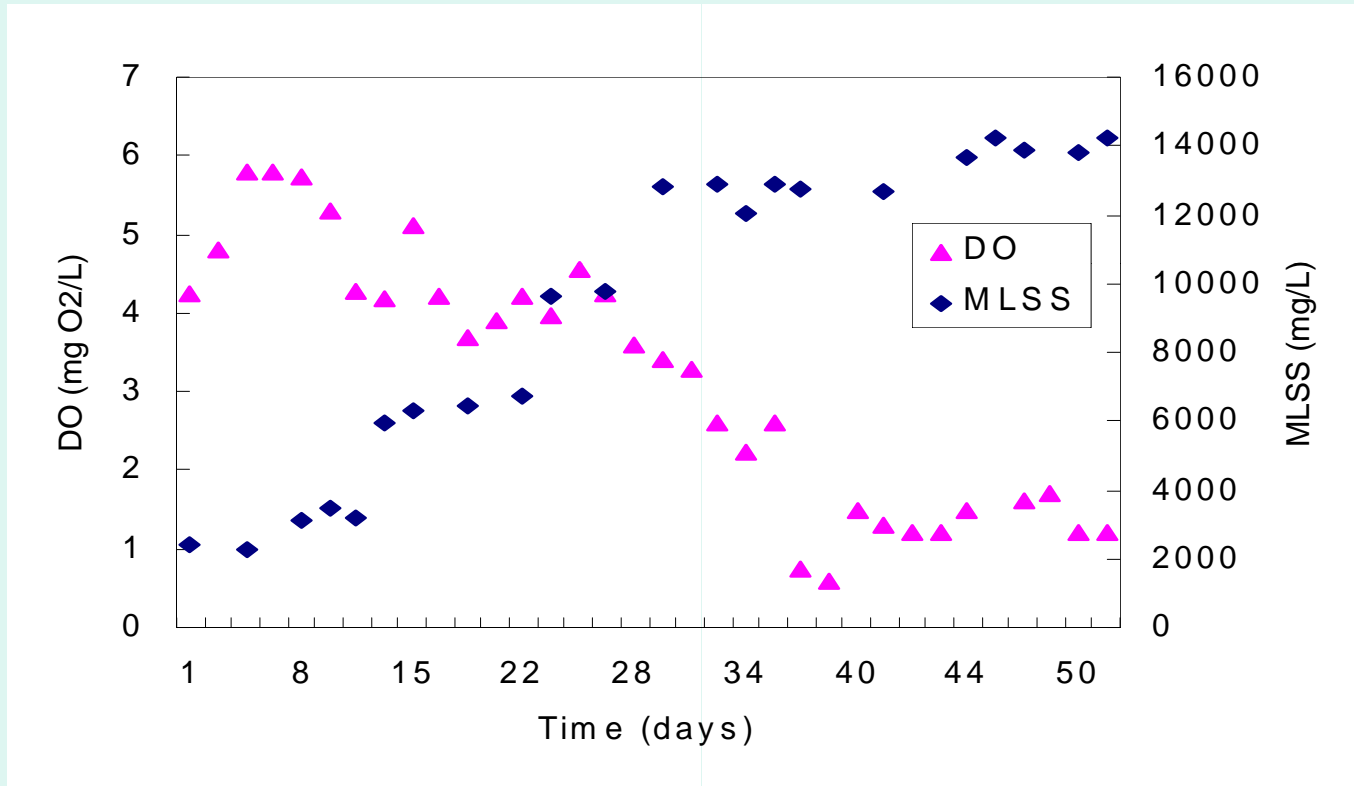
# Food Product Wastewater

## Influent and Effluent SS of Non-woven MBR



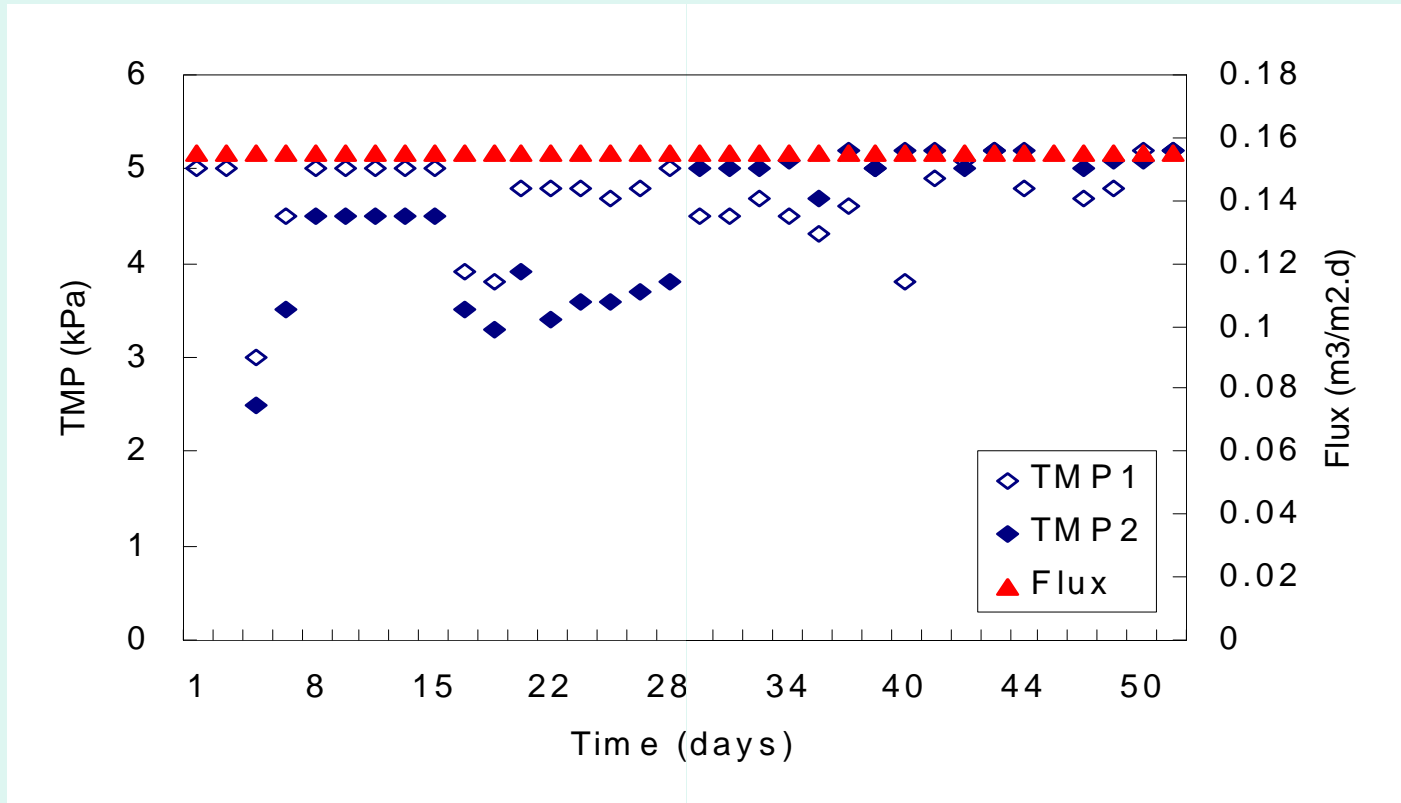
# Food Product Wastewater

## DO and MLSS of Non-woven MBR



# Food Product Wastewater

## Transmembrane pressure (TMP) and flux of non-woven MBR



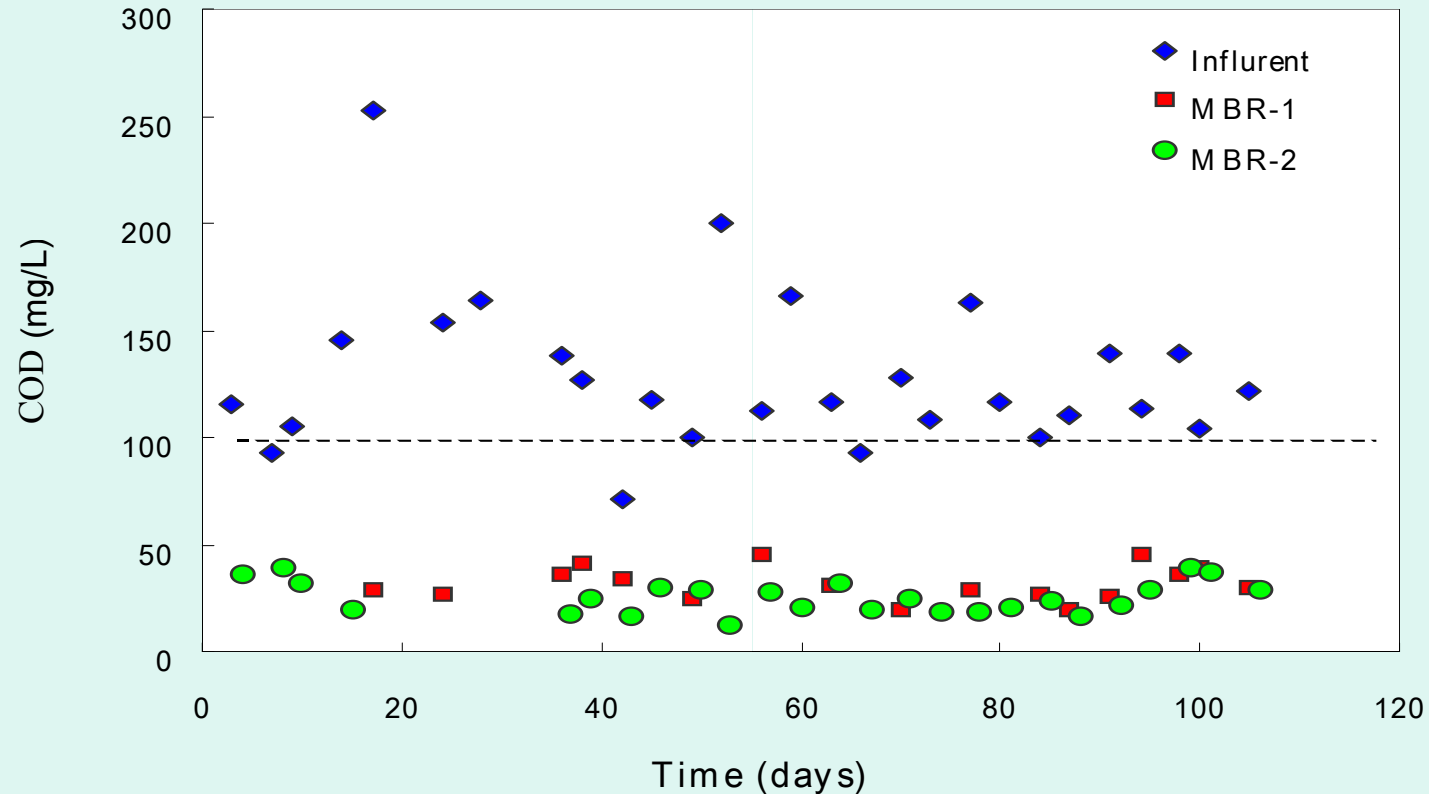
# Sewage Non-woven MBR Treatment

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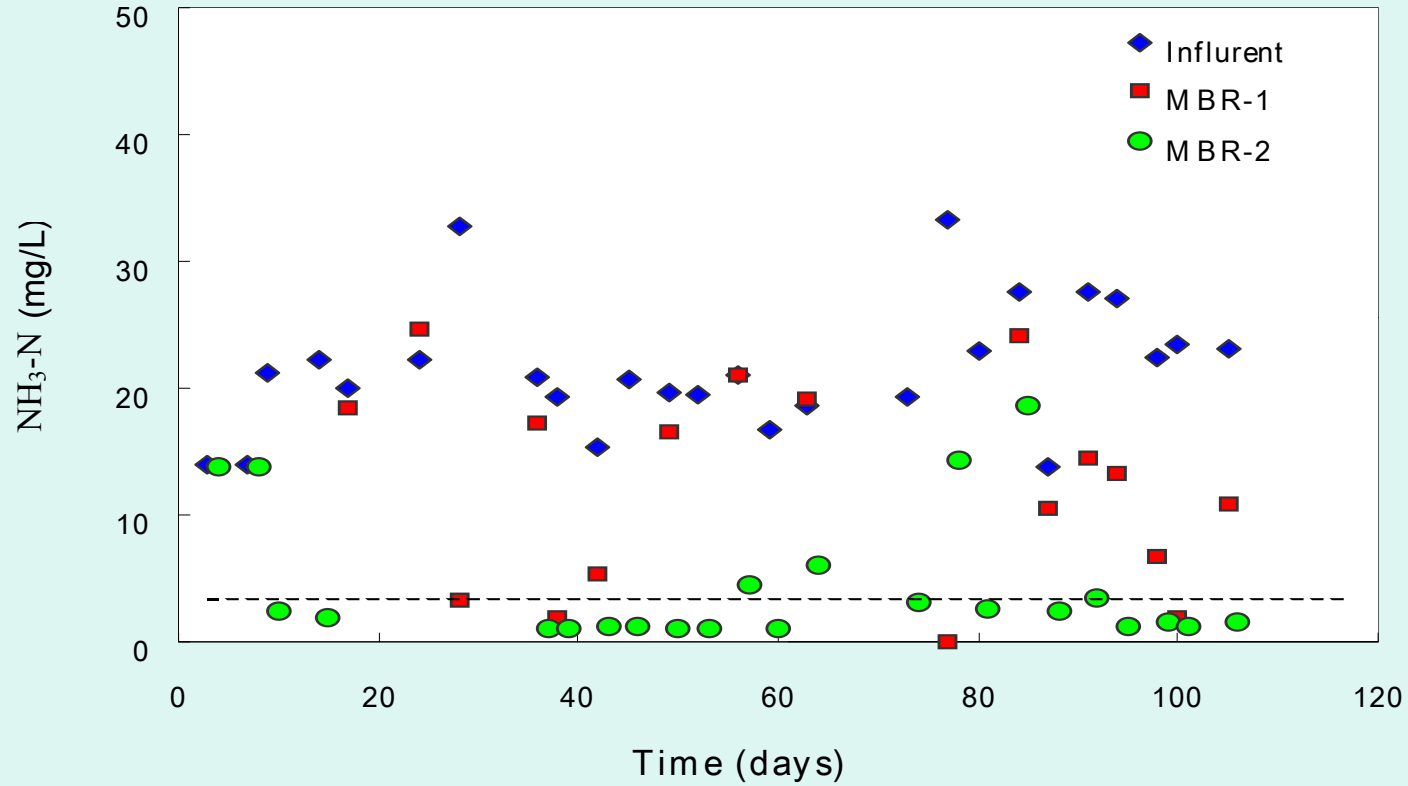
# Sewage Non-woven MBR Treatment

## COD removal



# Non-woven MBR Treatment

## NH<sub>3</sub>-N removal

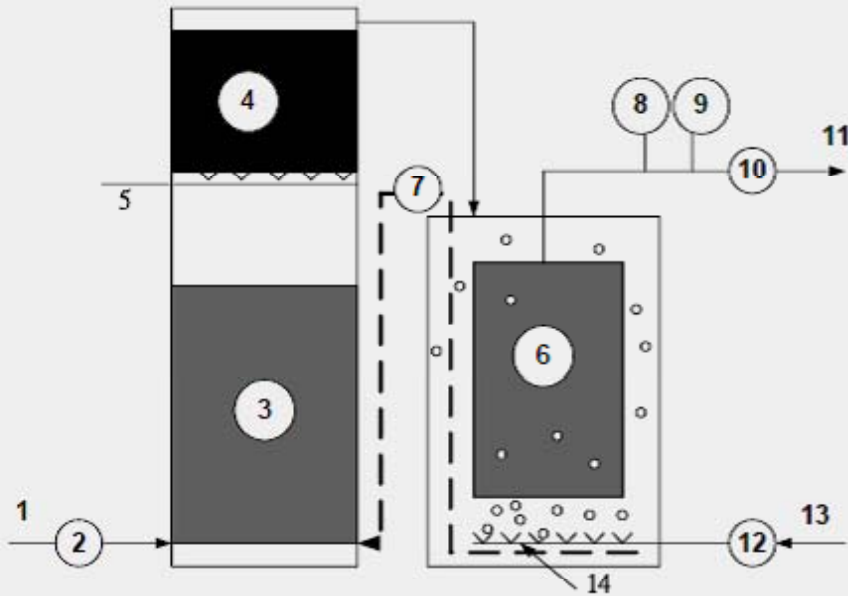


# Benefit of Non-woven MBR

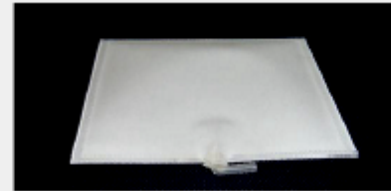
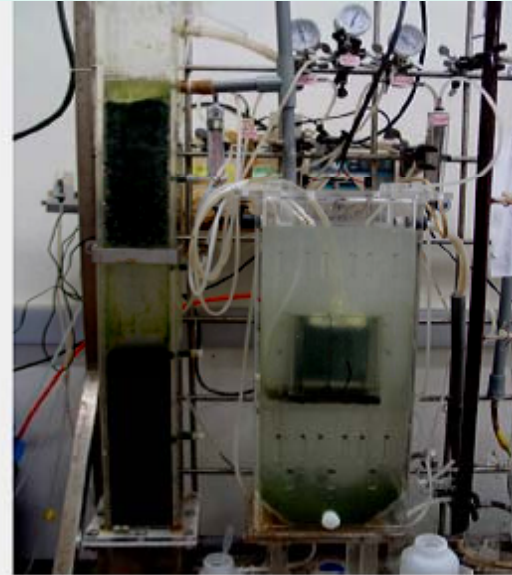
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- Low transmembrane pressure
- Advantage in membrane cost
- Low requirement of influent quality and operation

# Anaerobic Non-woven MBR process



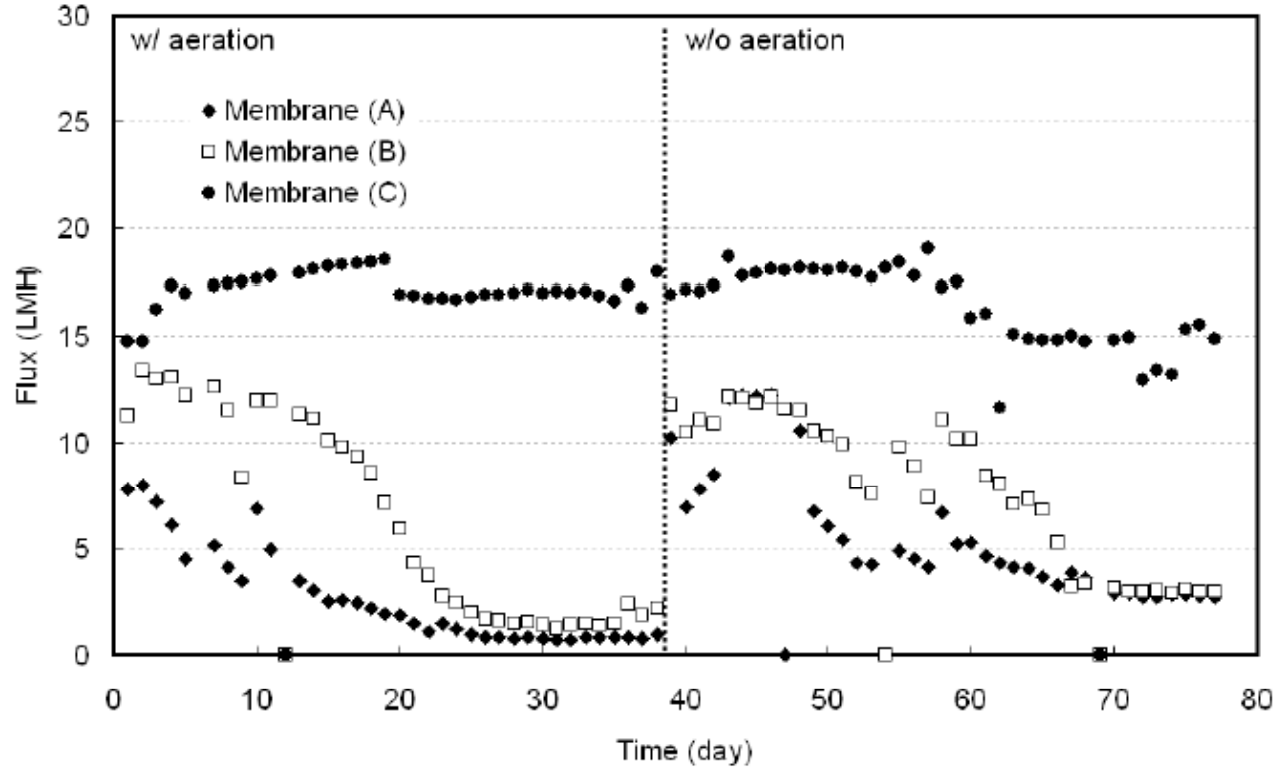
(1:進流水(influent)·2 :進料幫浦(influent pump)· 3:厭氧生物區(anaerobic zone), 4:不織布擔體區(non-woven carrier zone), 5:反沖洗裝置(back-wash)· 6:不織布薄膜分離區(non-woven membrane zone), 7: 污泥回流幫浦( sludge recycle pump), 8壓力表( pressure gauge)· 9:流量計(flow meter)· 10: 濾液幫浦(permeate pump), 11:濾液(permeate), 12 :曝氣裝置( blower), 13: 氣體(air)· 14 曝氣裝置(aeration device)



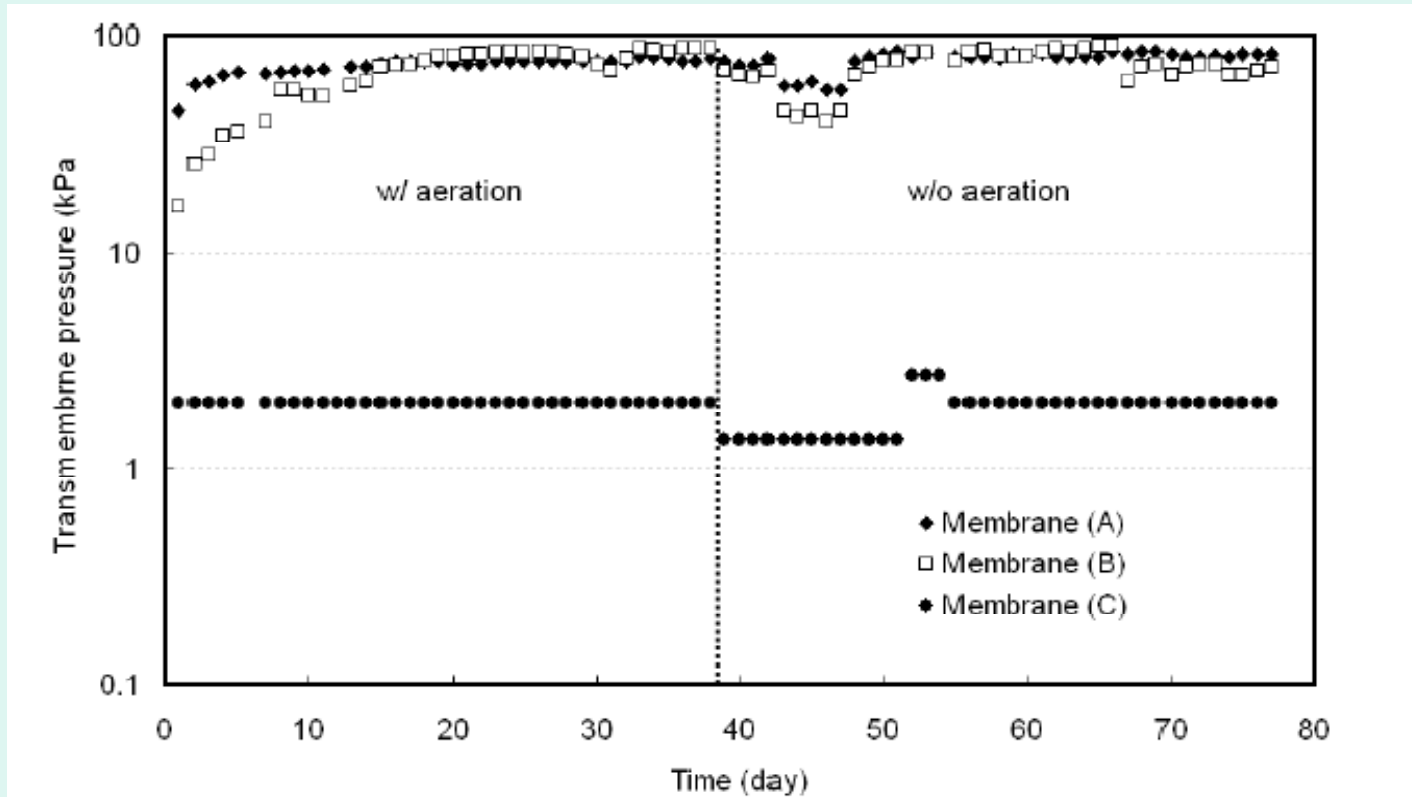
- Three different pore sizes of non-woven membrane i.e.
- 0.2 $\mu\text{m}$  (membrane A),
- 2.0 $\mu\text{m}$  (membrane B),
- 20.0 $\mu\text{m}$  (membrane c)

# Anaerobic Non-woven MBR process

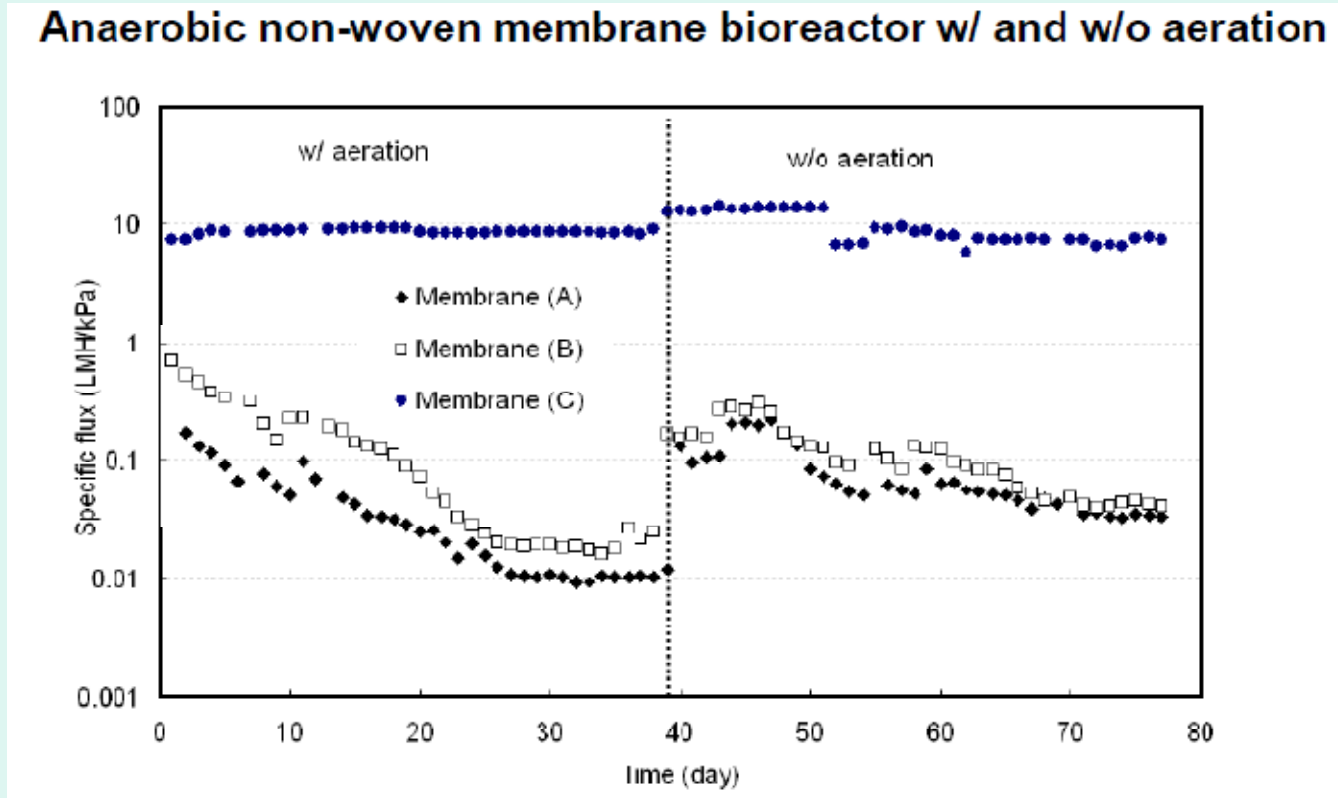
Anaerobic non-woven membrane bioreactor w/ and w/o aeration



# Anaerobic Non-woven MBR process

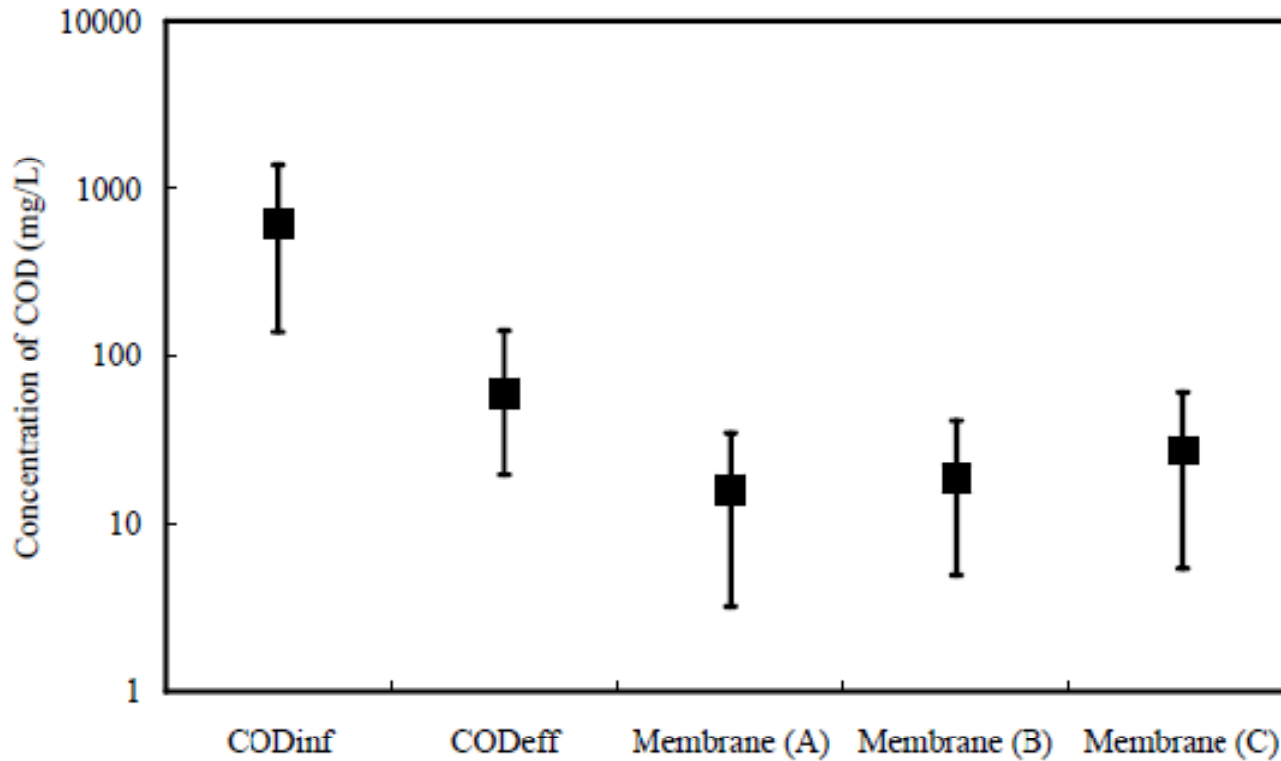


# Anaerobic Non-woven MBR process



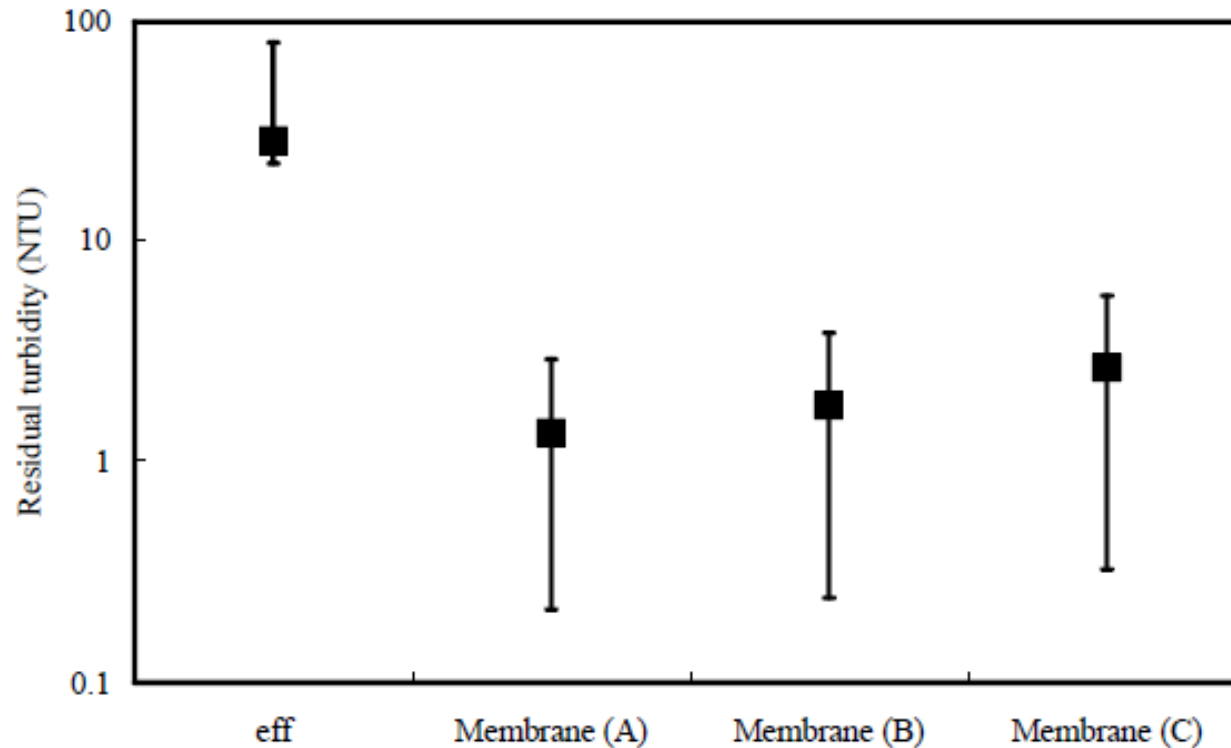
# Anaerobic Non-woven MBR process

COD of the effluent from UASB and three membrane modules



# Anaerobic Non-woven MBR process

Turbidity of the effluent from UASB and three membrane modules



# Anaerobic Non-woven MBR process

Analysis of scale substance on the surface of non-woven membrane

| foulants               | units                   | influent | Membrane A<br>(0.2 $\mu\text{m}$ ) | Membrane B<br>(2.0 $\mu\text{m}$ ) | Membrane C<br>(20.0 $\mu\text{m}$ ) |
|------------------------|-------------------------|----------|------------------------------------|------------------------------------|-------------------------------------|
| polysaccharide         | mg/L                    | 5.9      | 1.2                                | 3.5                                | 5.7                                 |
| protein                | mg/L                    | 0.21     | 0.07                               | 0.18                               | 0.20                                |
| Bicarbonate alkalinity | mg/L as $\text{CaCO}_3$ | 764      | 646                                | 707                                | 737                                 |
| calcium                | mg/L                    | 44.8     | 33.9                               | 37.6                               | 42.8                                |

# Conclusions

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- Non-woven textiles could be used as the filter material of **aerobic** and **anaerobic** MBR by properly selecting its pore size to get low membrane fouling.
- The filtration behavior of the non-woven MBR is different from those of conventional microporous MBR, especially operating at **high aeration intensity** and **high MLSS** concentration.
- **Anaerobic non-woven MBR**, **which saving much aeration energy for biodegradation and membrane scouring**, shows that will be a promising technology for industrial wastewater treatment.

# Acknowledgements

- ITRI team would like to thank Taiwan KNH Company for a complete cooperation and help on non-woven MBR and relative research and development works.



<http://www.itriwater.org.tw/>